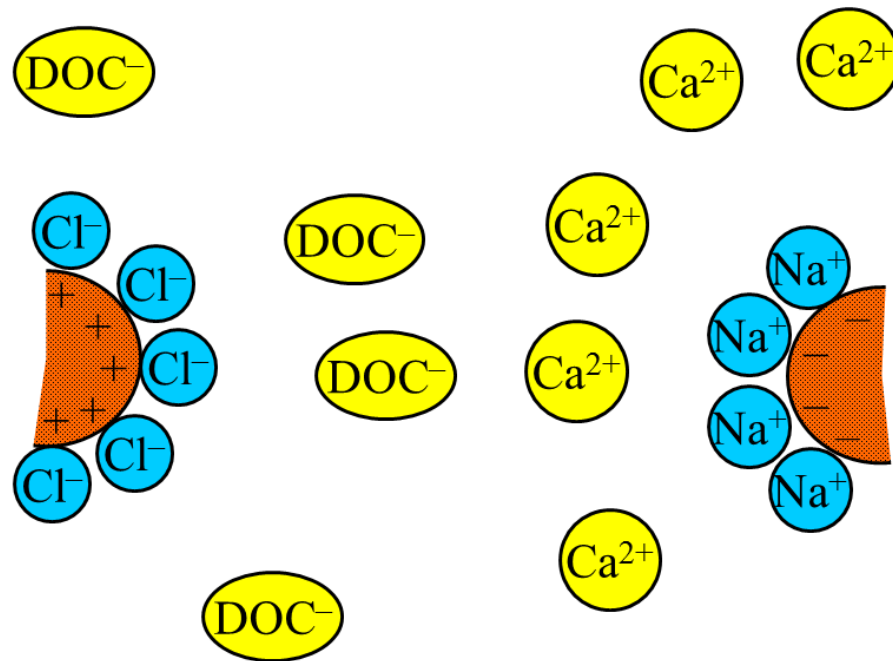


# Combined Ion Exchange for Removal of Dissolved Organic Carbon and Hardness

Treavor Boyer  
30 August 2016



# Acknowledgements



**Small, Safe, Sustainable (S3) Public Water Systems through Innovative Ion Exchange (R835334)**



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**Many great students – Jennifer Apell, Katie Indarawis, Sarah Comstock, Gabe Maul, Jerrine Foster, Yue Hu, Alysse Ness**



**Dr. Qiong (Jane) Zhang**



**Cedar Key Water & Sewer District**



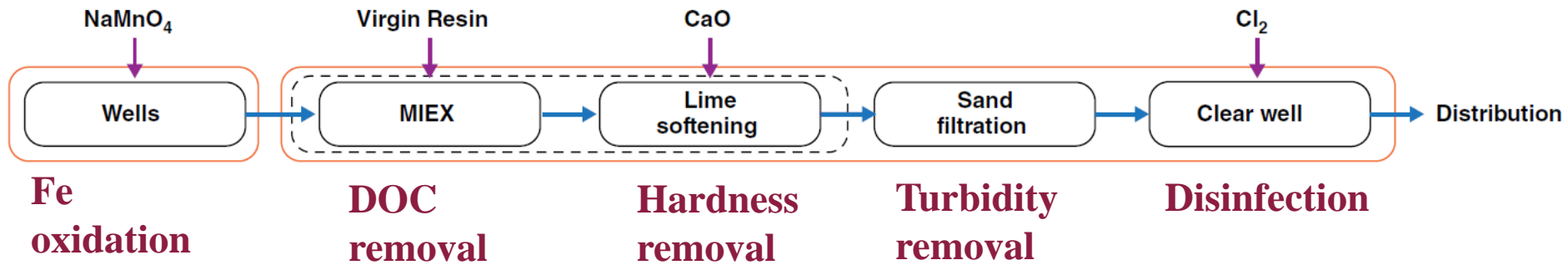
# Challenges faced by small water systems

Oxenford & Barrett, 2016. Understanding Small Water System Violations and Deficiencies. *Journal AWWA*, 108(3), 31–37.

- Management and operations
- Source water
- Security
- Pumps
- Compliance
- Data verification
- Treatment
- Finished water storage
- Distribution
- Financial

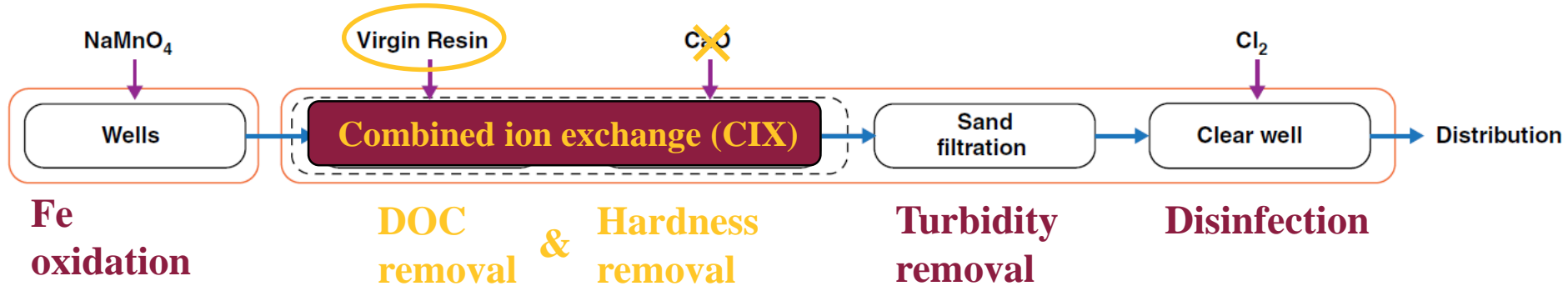
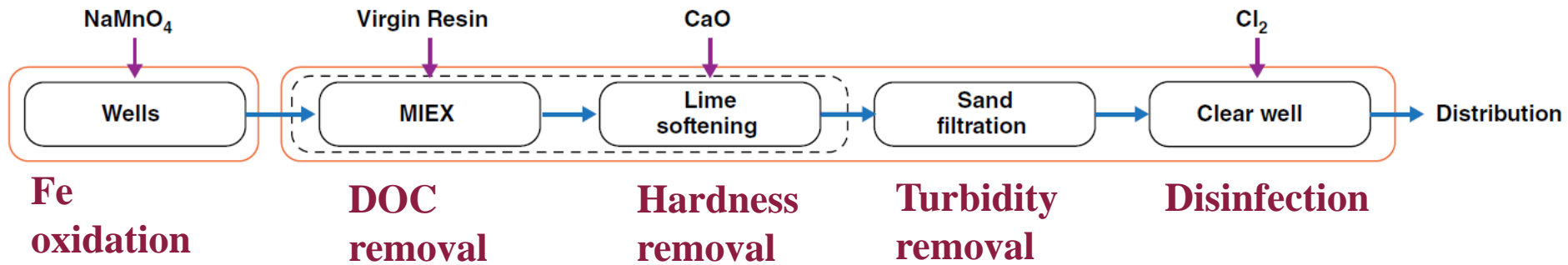
# Challenges faced by small water systems

- Process
- Energy
- Water
- Chemicals



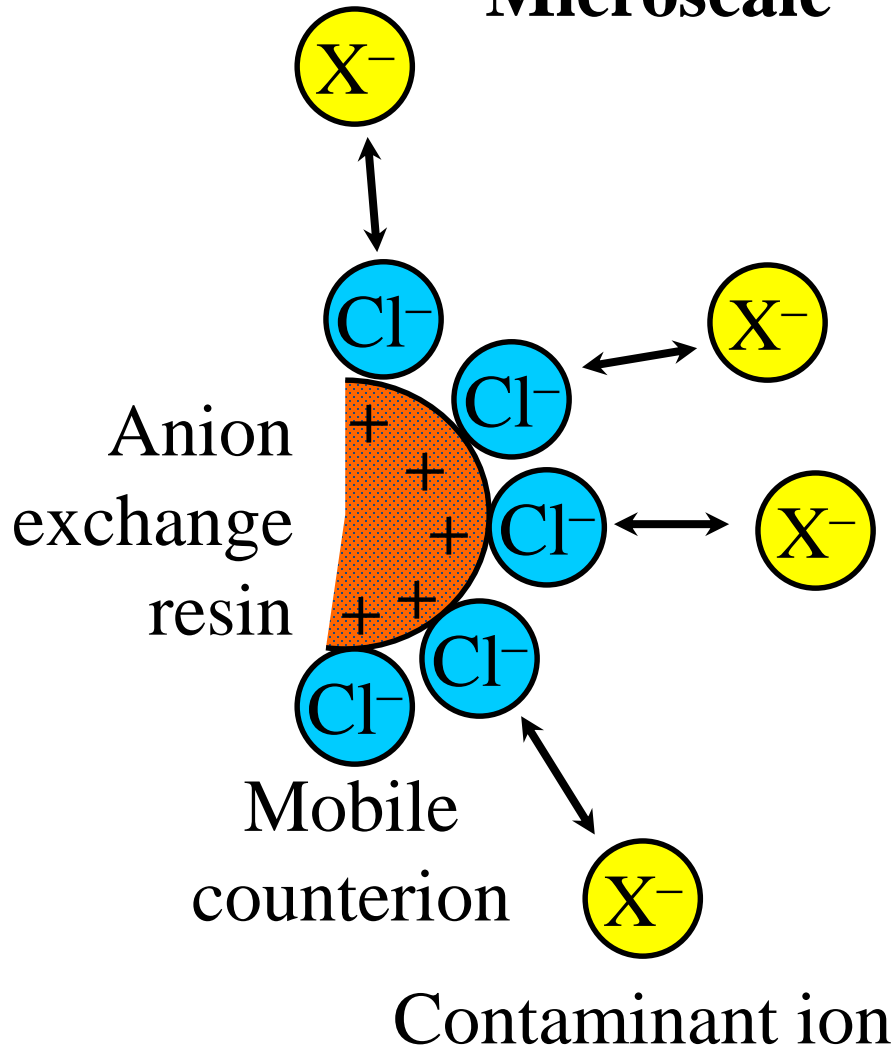
# Challenges faced by small water systems

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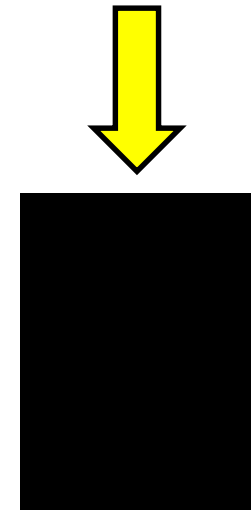
# Ion exchange

**Microscale**



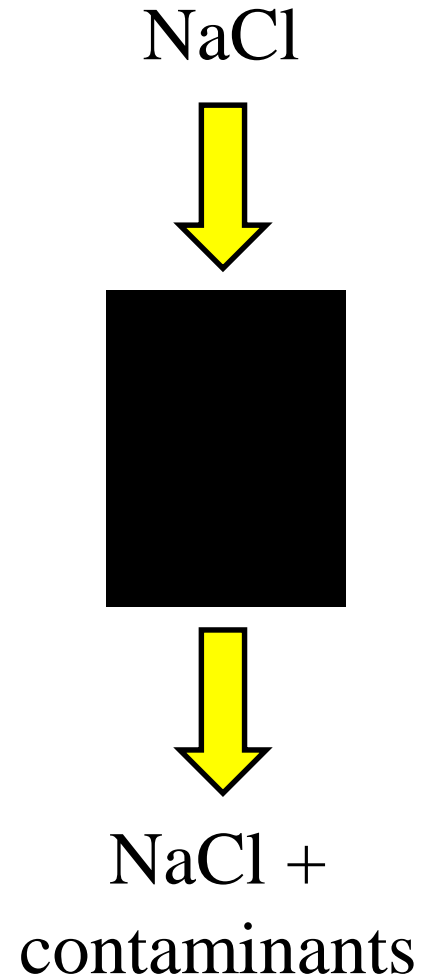
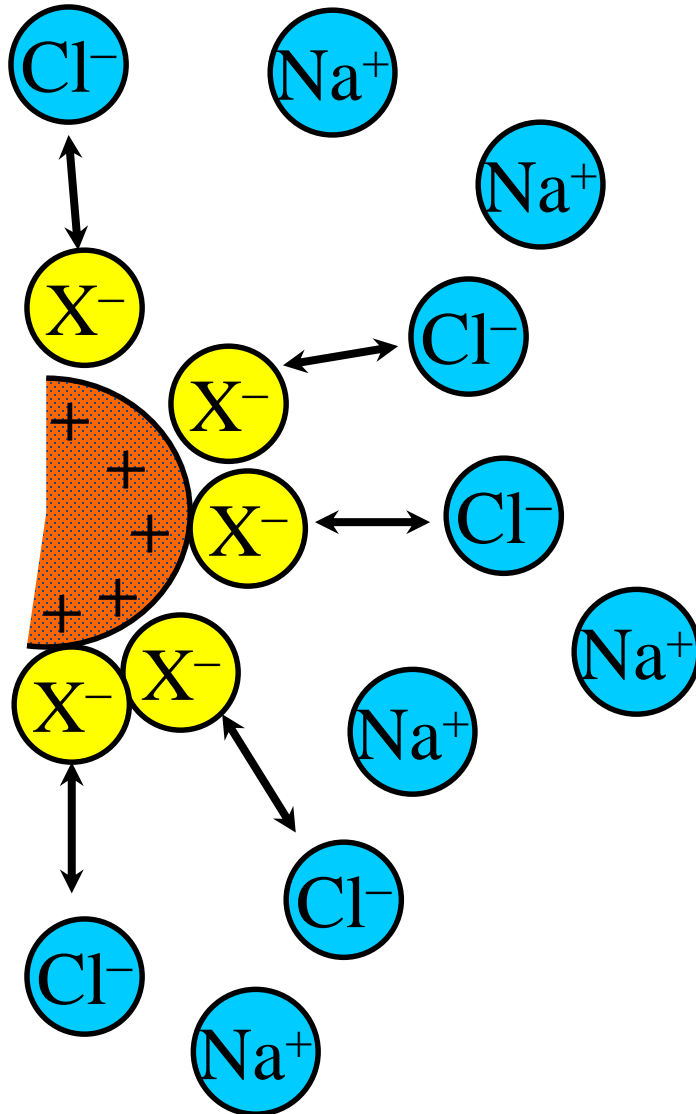
**Macroscale**

Contaminant

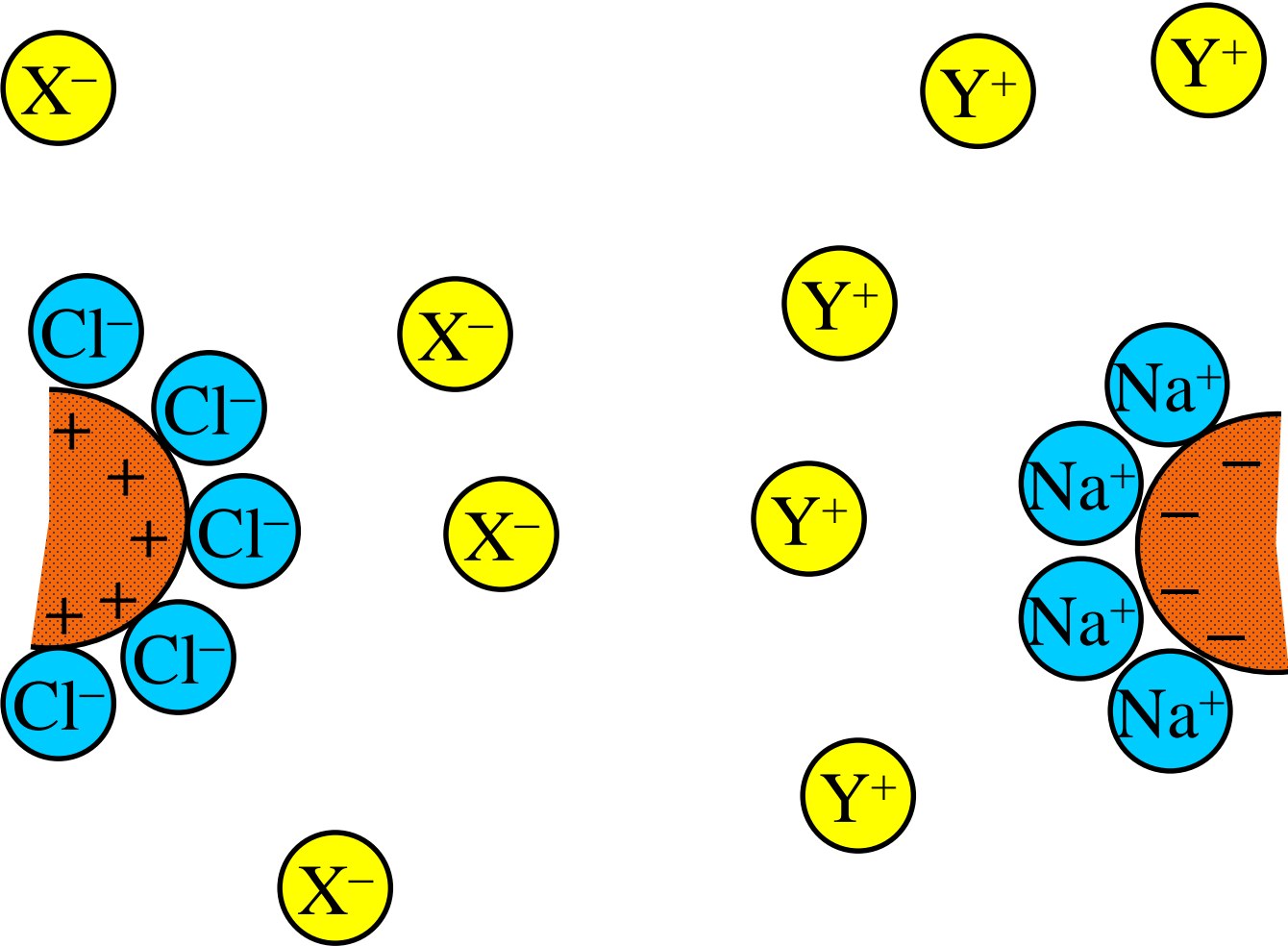


Contaminant-free

# Regeneration

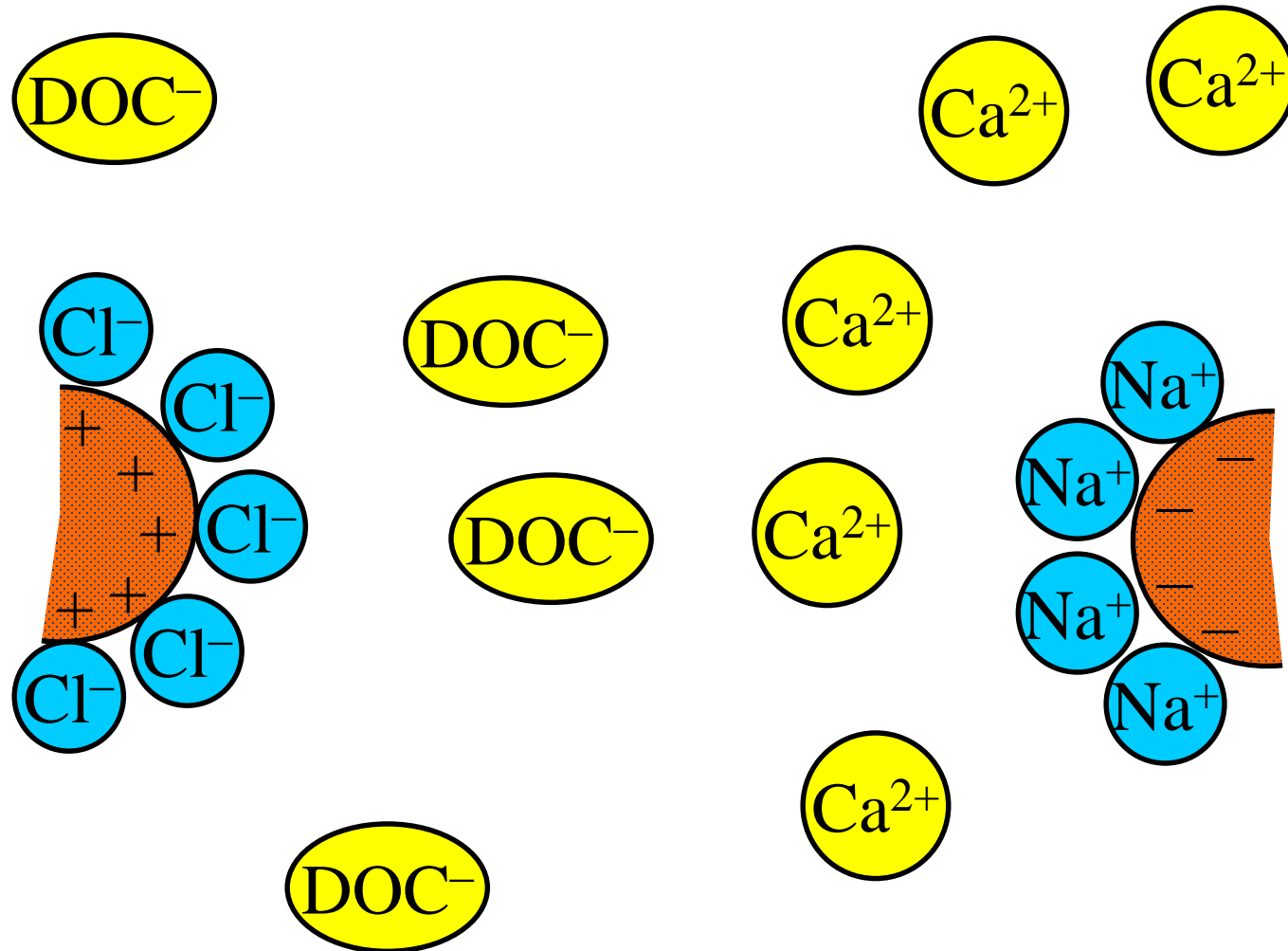


# Combined ion exchange (CIX)

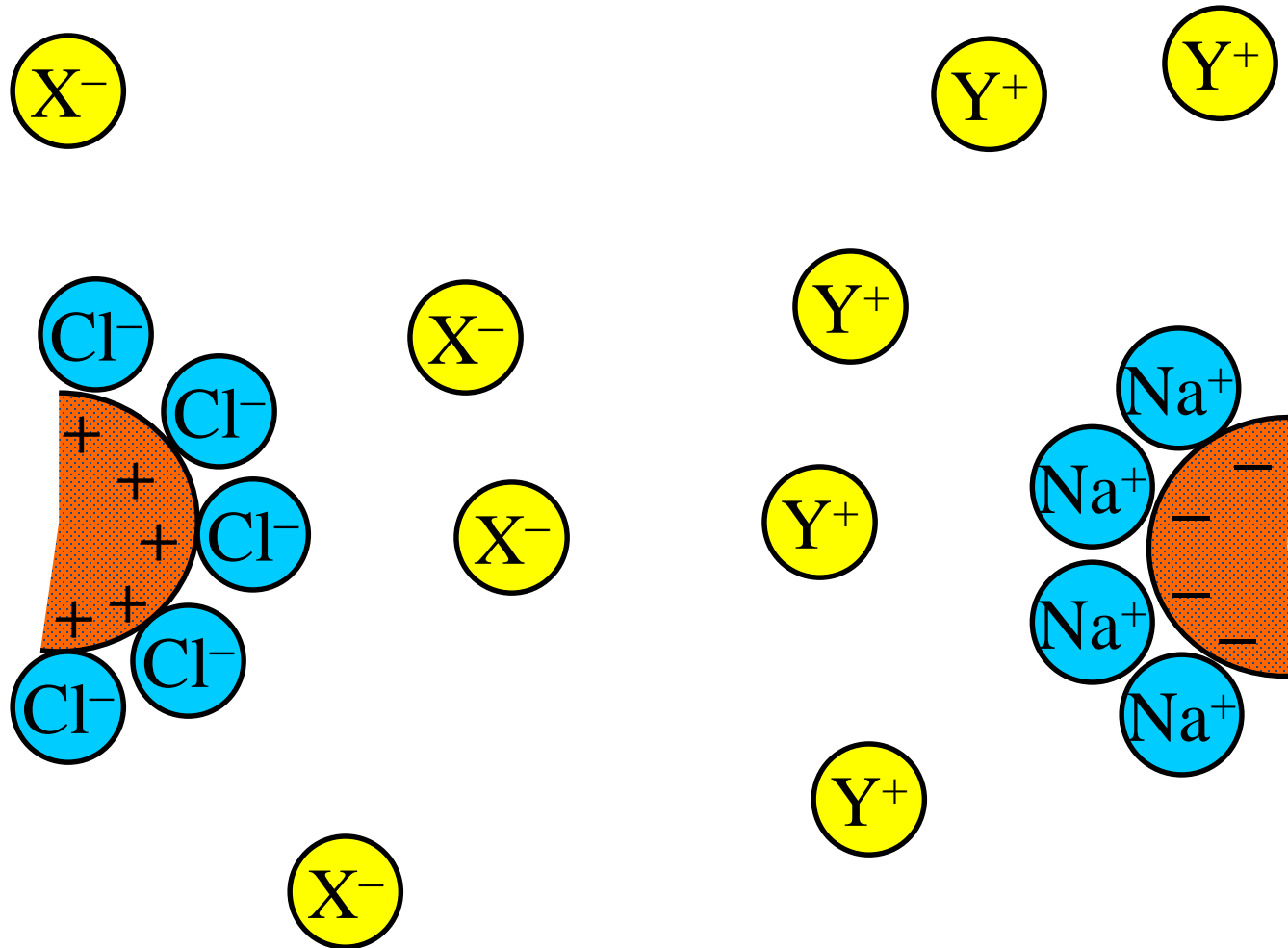




# CIX: DOC and hardness removal

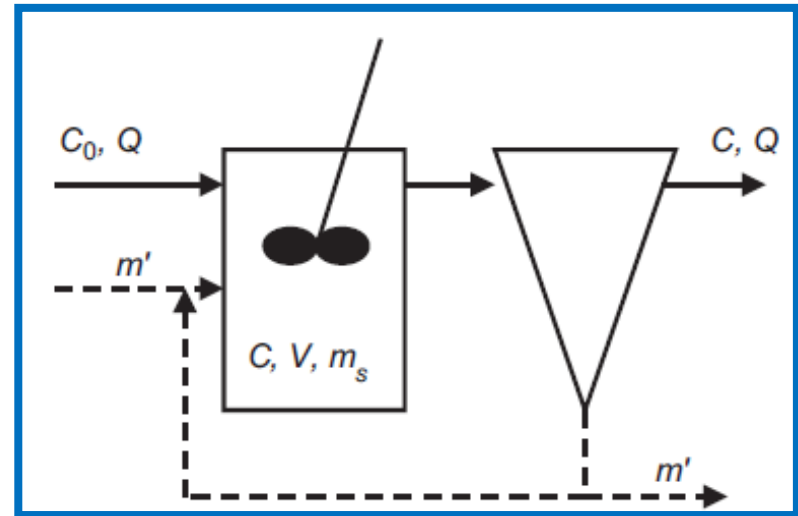
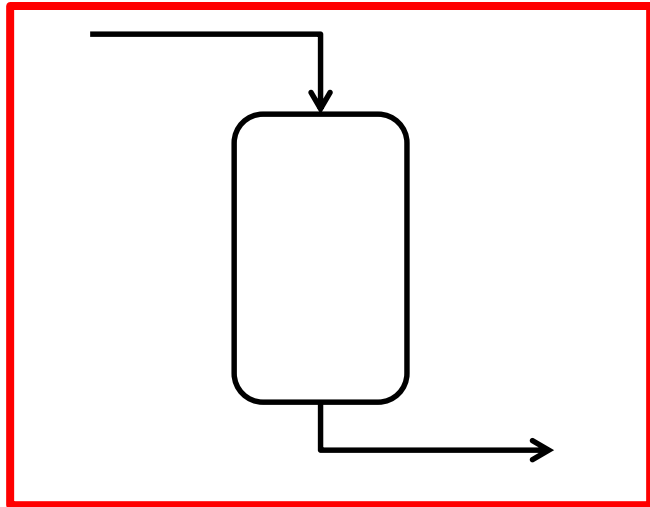


# CIX & multi-contaminant removal



# Ion exchange reactors

- Fixed bed reactor
- Completely mixed reactor with resin recycle



# Proof of concept

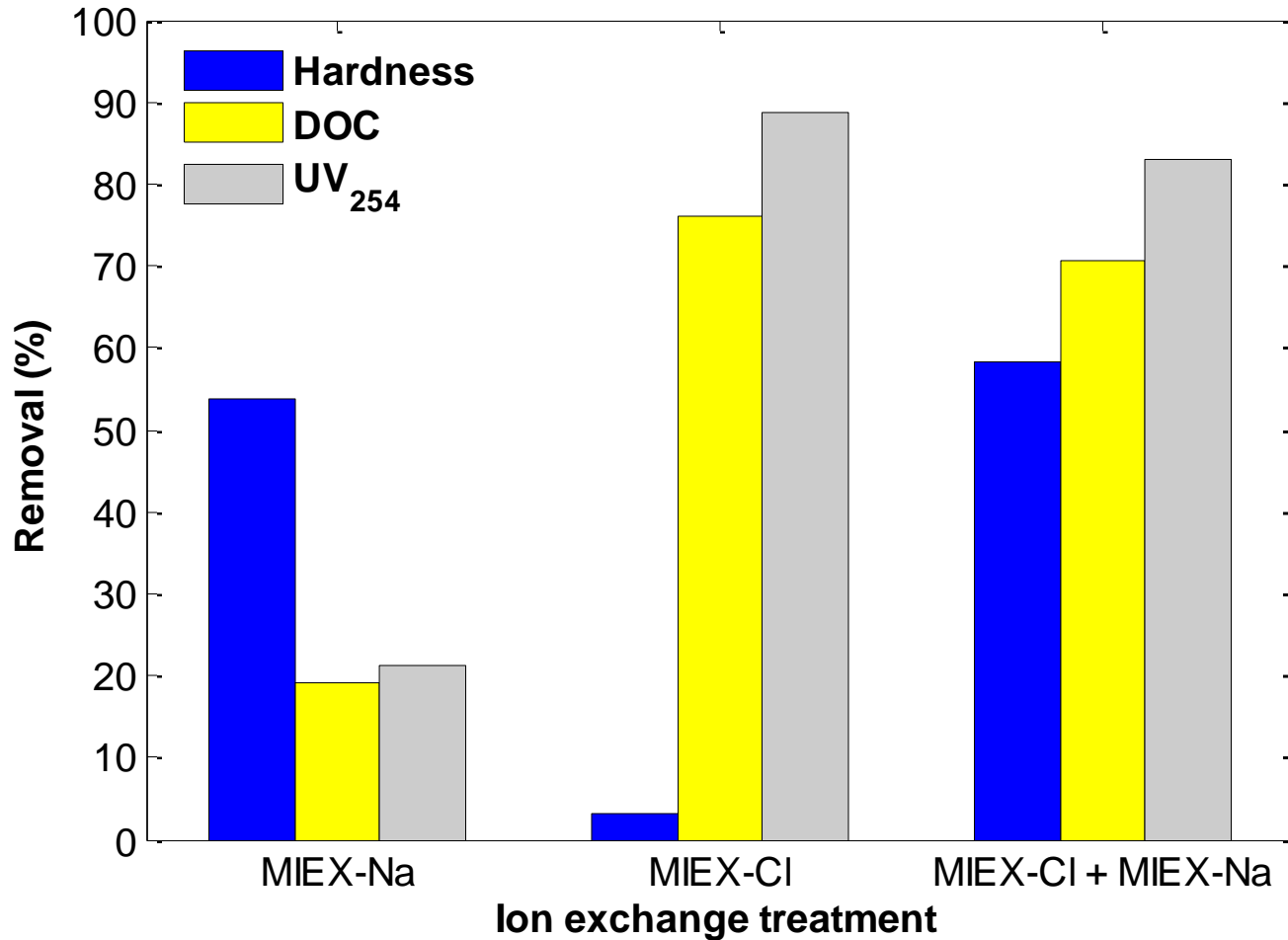
- Apell, J.N., Boyer, T.H., 2009. Simultaneous removal of dissolved organic matter and hardness by combined ion exchange. *AWWA Water Quality Technology Conference and Exposition* Seattle, Washington, 15–18 November 2009, 8 p.
- Apell, J.N., Boyer, T.H., 2010. Combined ion exchange treatment for removal of dissolved organic matter and hardness. *Water Research* 44, 2419–2430.

# Proof of concept

## Experimental design

- Groundwater from Cedar Key
  - DOC: 5.6 mg/L
  - Hardness: 275 mg/L as  $\text{CaCO}_3$
- Anion exchange resin: 2 mL/L MIEX-Cl
- Cation exchange resin: 16 mL/L MIEX-Na
- Single-loading jar tests
  - Simultaneous: MIEX-Cl + MIEX-Na
  - Sequence 1: MIEX-Cl  $\rightarrow$  MIEX-Na
  - Sequence 2: MIEX-Na  $\rightarrow$  MIEX-Cl
- NaCl regeneration

# Proof of concept



- 70% DOC removal and 55% hardness removal

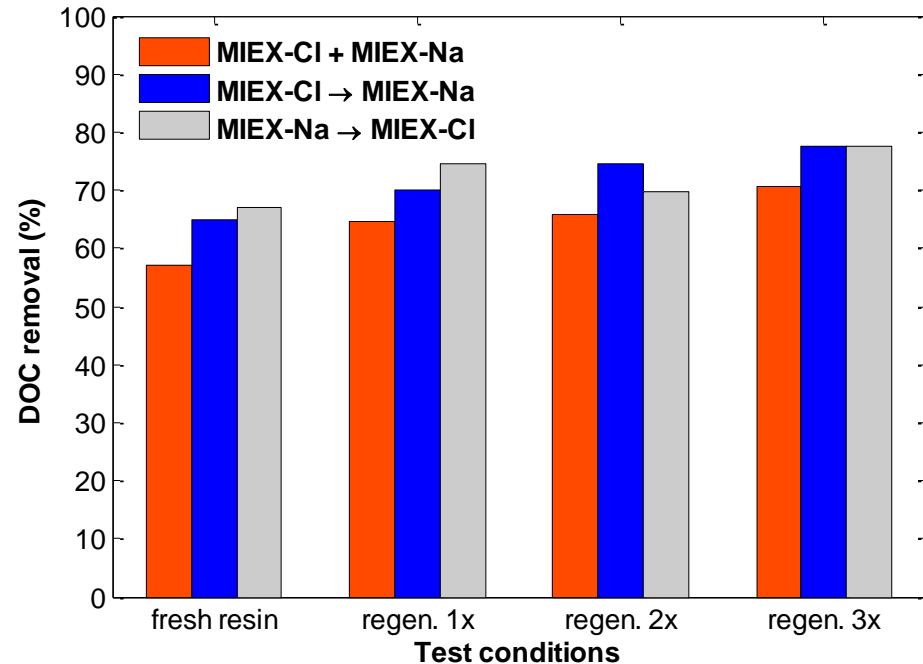
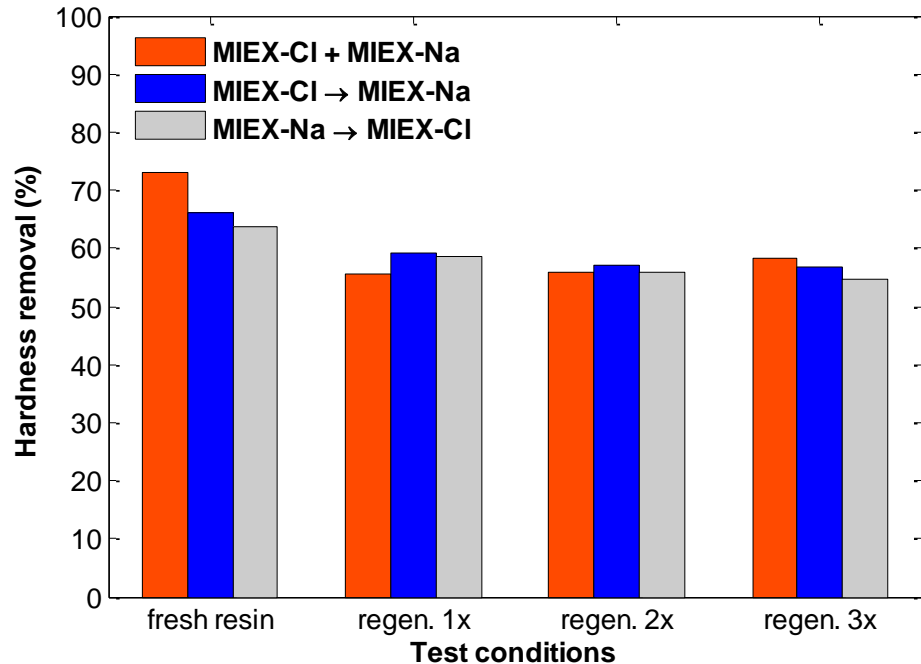
# Proof of concept

| Parameter                             | MIEX-Cl + MIEX-Na | Finished drinking water <sup>a</sup> |
|---------------------------------------|-------------------|--------------------------------------|
| pH                                    | 7.7               | 8.1                                  |
| DOC (mg C/L)                          | 1.7               | 1.1                                  |
| Hardness (mg/L as CaCO <sub>3</sub> ) | 112               | 173                                  |
| Chloride (mg/L)                       | 49                | 60                                   |
| Sulfate (mg/L)                        | 3.1               | 1.1                                  |

<sup>a</sup> Cedar Key Water & Sewer District; August 2009.

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# Proof of concept



- Decrease in hardness removal and increase in DOC removal after 3 regeneration cycles
- Simultaneous and sequential ion exchange showed similar removals after 3 regeneration cycles



# Proof of concept

## Conclusions

- MIEX-Cl and MIEX-Na can be used in a single completely mixed vessel to simultaneously remove DOC and hardness
- MIEX-DOC and MIEX-Ca can be effectively regenerated using NaCl in a single completely mixed vessel
- Simultaneous and sequential ion exchange showed approximately equal removal after three regeneration cycles
- NaCl regeneration solution prepared using tap water (i.e., containing hardness and alkalinity) provided the same regeneration efficiency as NaCl regeneration solution prepared using hardness-free, deionized water

# Proof of concept

## Observations

- MIEX-Na removed DOC in addition to hardness. This was unexpected because DOC is negatively charged.
- Combined ion exchange is expected to be an effective pretreatment to reduce membrane fouling, i.e., decrease organic fouling by DOC and inorganic scaling by calcium minerals

# Focus on cation exchange

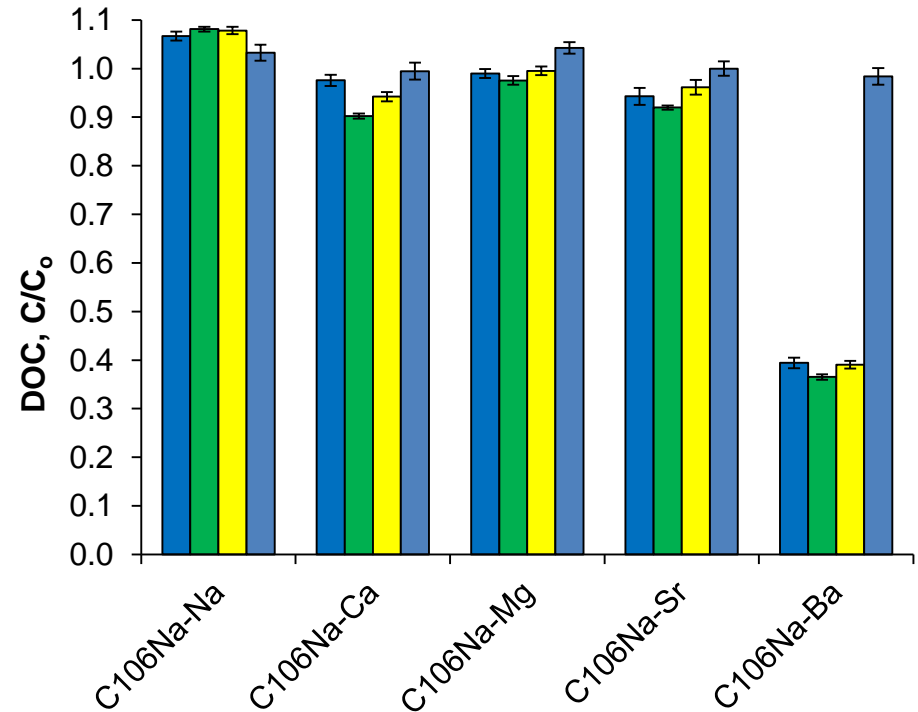
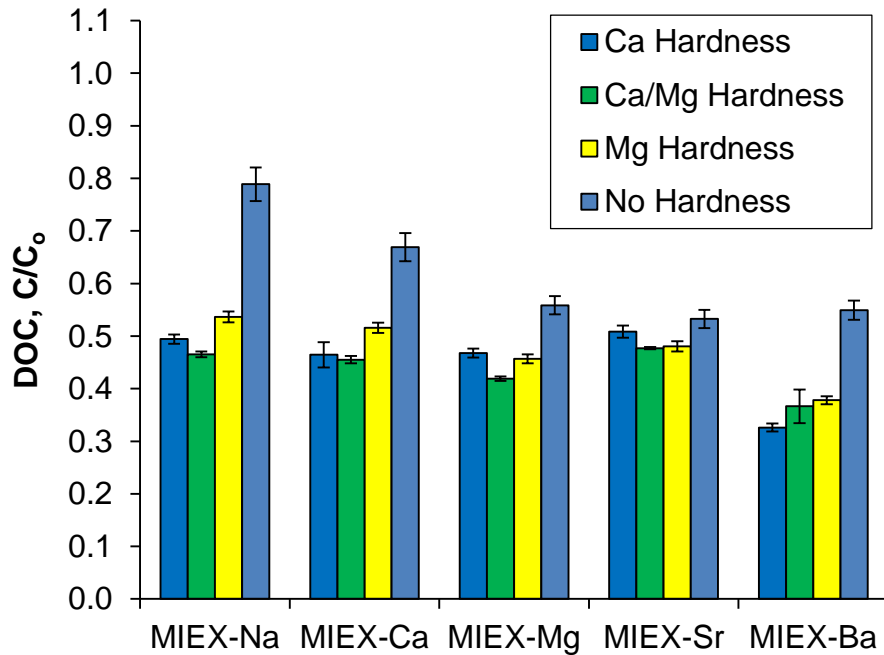
- Indarawis, K.A., Boyer, T.H., 2012. Alkaline earth metal cation exchange: Effect of mobile counterion and dissolved organic matter. *Environmental Science & Technology* 46, 4591–4598.
- Indarawis, K.A., Boyer, T.H., 2013. Superposition of anion and cation exchange for removal of natural water ions. *Separation and Purification Technology*, 118, 112–119.
- Indarawis, K.A., Boyer, T.H., 2014. Evaluation of ion exchange pretreatment options to decrease fouling of a reverse osmosis membrane. *Desalination and Water Treatment*, 52(25–27), 4603–4611.

# Focus on cation exchange

## Experimental design

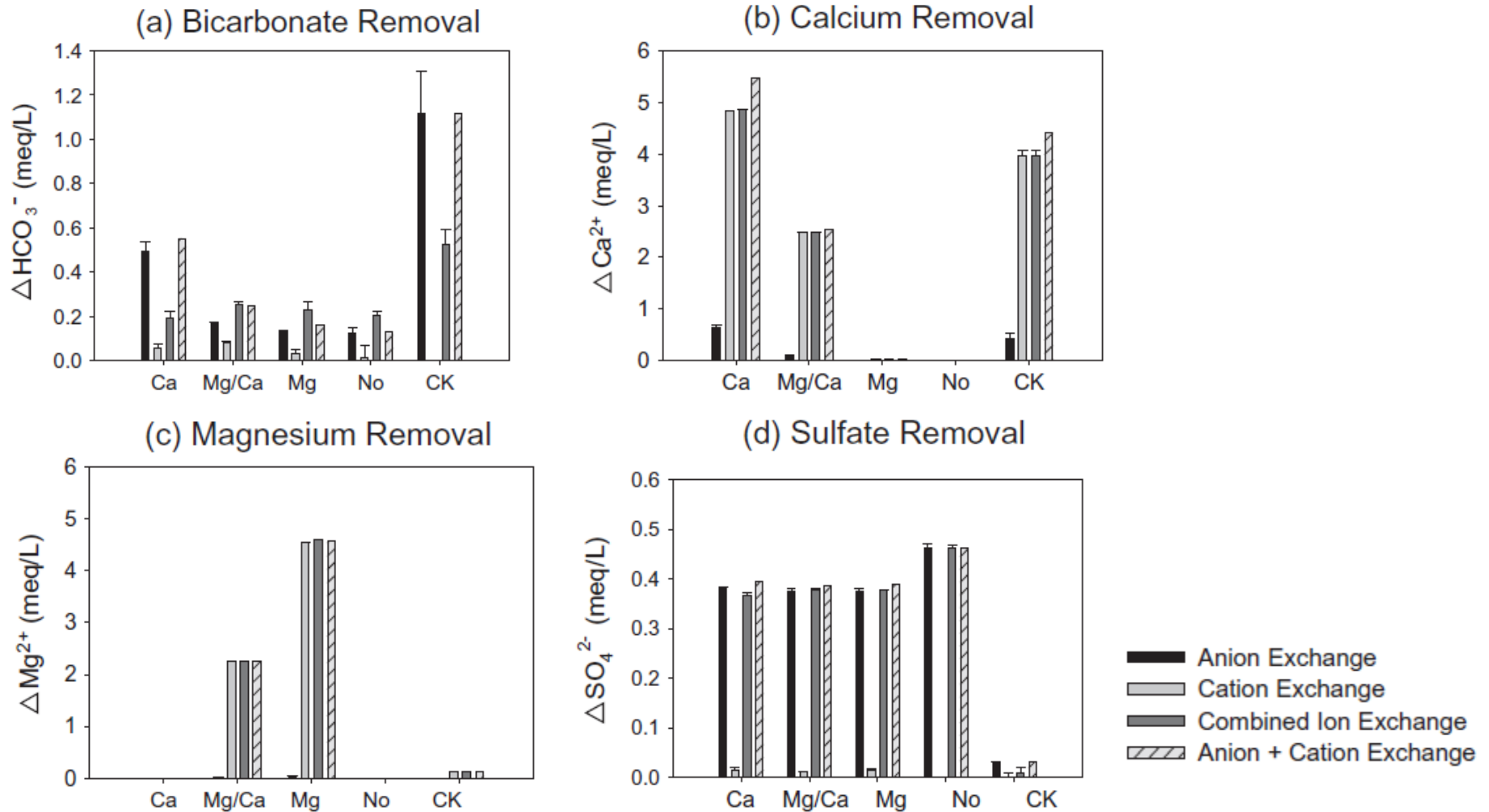
- Synthetic water to mimic Cedar Key groundwater
  - Suwannee River NOM (~5 mg/L DOC)
  - Hardness as  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{Ca}^{2+}/\text{Mg}^{2+}$  (~250 mg/L as  $\text{CaCO}_3$ )
- Cation exchange resin
  - 16 mL/L MIEX-Na
  - 3.1 mL/L Purolite C106-Na
  - Resin-Na, -Ca, -Mg, -Sr, and -Ba
- Batch equilibrium experiments

# Focus on cation exchange



- DOC removal by magnetic cation exchange resin
- No DOC removal by non-magnetic cation exchange resin

# Combined ion exchange, revisited



- Combined ion exchange is additive

# Focus on cation exchange

## Conclusions

- DOC removal was approximately 20% for MIEX-Na resin with no hardness cations in solution
- DOC removal by MIEX resin increased when the presaturant ion was a divalent metal cation or divalent metal cation was present in solution or both
- There was no measureable DOC removal by the non-magnetic cation exchange resin for all conditions of presaturant ion and metal cations in solution, with the exception of barium as the presaturant ion
- Combined ion exchange is additive

# Combined ion exchange (CIX)

- Comstock, S.E.H., Boyer, T.H., 2014. Combined magnetic ion exchange and cation exchange for removal of DOC and hardness. *Chemical Engineering Journal*, 241, 366–375.

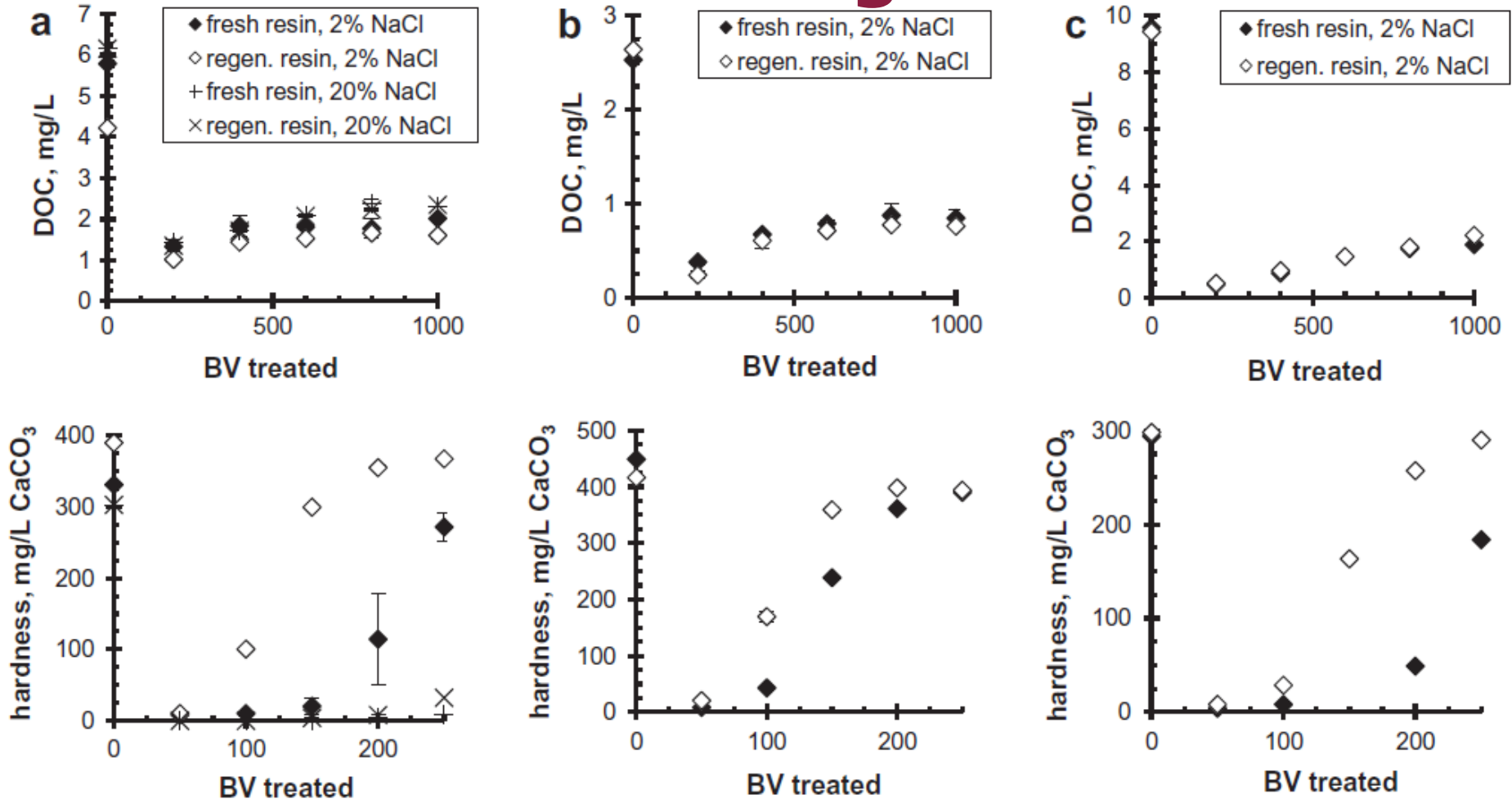


# CIX treatment of groundwater

## Experimental design

- Cedar Key, Yankeetown, Palm Springs groundwater
  - DOC: 3–10 mg/L
  - Hardness: 300–440 mg/L as  $\text{CaCO}_3$
- Anion exchange resin: MIEX-Cl
- Cation exchange resin: Amberlite 200C-Na
- Multiple-loading jar tests
  - Bed volumes (BV<sub>s</sub>)
  - 1000 BV<sub>s</sub> MIEX-Cl
  - 250 BV<sub>s</sub> A200C-Na
- NaCl regeneration (2%, 20%)

# CIX treatment of groundwater



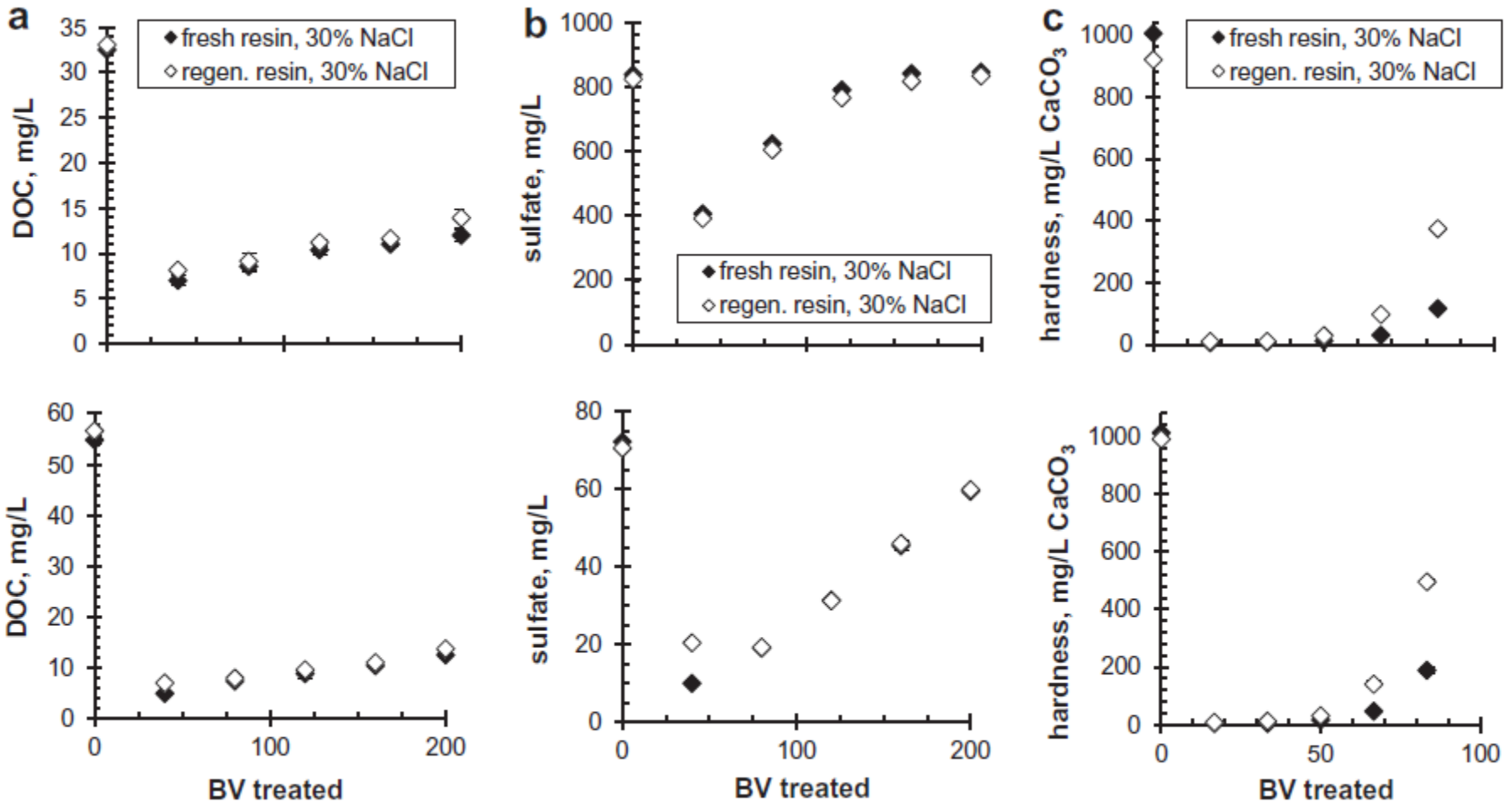
- 67–85% DOC removal, 1000 BV anion exchange (composite)
- ~50% hardness removal, 250 BV cation exchange (composite)

# CIX treatment of NF concentrate

## Experimental design

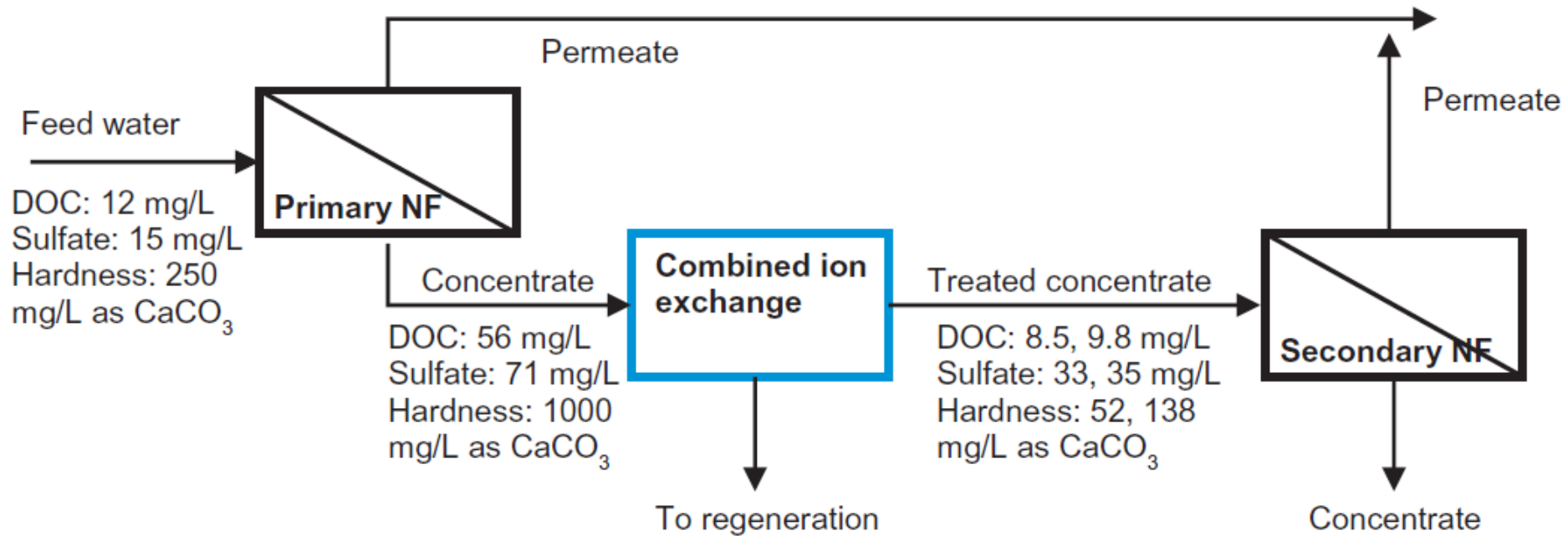
- NF concentrate from 2 membrane plants in FL
  - DOC: 33, 56 mg/L
  - Hardness: 960, 1000 mg/L as  $\text{CaCO}_3$
  - Sulfate: 830, 71 mg/L
- Anion exchange resin: MIEX-Cl
- Cation exchange resin: Amberlite 200C-Na
- Multiple-loading jar tests
  - 200 BVs MIEX-Cl
  - 83 BVs A200C-Na
- NaCl regeneration (30%)

# CIX treatment of NF concentrate



- 70–80% DOC removal, 50% sulfate removal, 90% hardness removal

# Primary NF – CIX – Secondary NF



- CIX produced similar water composition as NF feed water

# CIX

## Conclusions

- CIX treatment of groundwater achieved >70% DOC removal (MIEX-Cl resin) and >50% hardness removal (A200C-Na resin) in composite samples corresponding to 1000 BVs of anion exchange and 250 BVs of cation exchange depending on 2% or 20% NaCl regeneration solution
- CIX removed DOC, sulfate, and hardness from NF concentrate to produce treated concentrate with similar characteristics as NF feed water

# Combined ion exchange (CIX) pilot plant



# CIX pilot plant

## Experimental design

- Cedar Key
  - DOC: ~5 mg/L
  - Hardness: ~300 mg/L as CaCO<sub>3</sub>
- Anion exchange resin (AER): A-72 Thermax
- Cation exchange resin (CER): T-42 Thermax
- Pilot plant operation
  - Down flow columns
  - Resin ratio: 4 L AER-to-4 L CER
  - 0.5 gpm
- Regeneration: NaCl vs KCl regeneration (12% m/v)

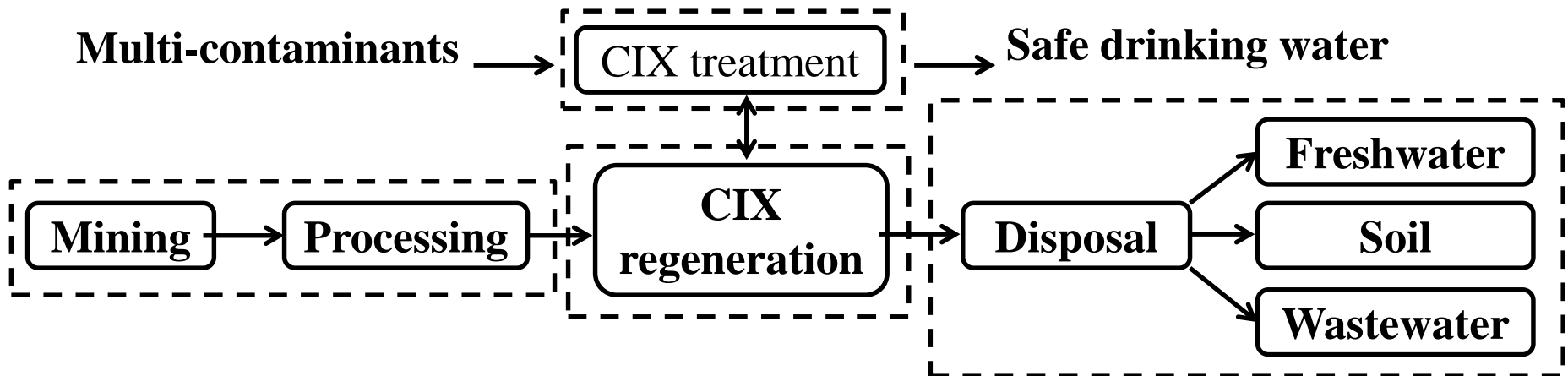


# CIX pilot plant, ongoing work

- Regeneration operation, e.g., precipitation
- Effectiveness of NaCl vs. KCl regeneration; disposal
- Lead–lag column operation
- Completely mixed CIX
- NaCl vs. NaHCO<sub>3</sub> regeneration (anion exchange only)
- Process modeling (w/ USF, WINSSS)
- Life cycle assessment (w/ USF, WINSSS)
- Decision support tool (w/ USF, WINSSS)

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# Thank you

**Treavor Boyer**  
**Arizona State University**  
**thboyer@asu.edu**

## Other resource on Ion Exchange and CIX

- Hu, Y., Foster, J., Boyer, T.H., 2016. Selectivity of bicarbonate-form anion exchange for drinking water contaminants: Influence of resin properties. *Separation and Purification Technology*, 163, 128–139.
- Boyer, T.H., 2015. Removal of dissolved organic matter by magnetic ion exchange resin. *Current Pollution Reports*, 1(3), 142–154.
- Zhang, J., Amini, A., O'Neal, J.A., Boyer, T.H., Zhang, Q., 2015. Development and validation of a novel modeling framework integrating ion exchange and resin regeneration for water treatment. *Water Research*, 84, 255–265.
- Maul, G.A., Kim, Y., Amini, A., Zhang, Q., Boyer, T.H., 2014. Efficiency and life cycle environmental impacts of ion-exchange regeneration using sodium, potassium, chloride, and bicarbonate salts. *Chemical Engineering Journal*, 254, 198–209.